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Photodegradation of Orange II under visible light using Cu–Ni/TiO₂: Effect of calcination temperature

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ABSTRACT

The decolorization of Orange II was studied under visible light using bimetallic Cu-Ni/TiO₂ prepared via precipitation method. Photocatalysts with different Cu:Ni mass compositions were prepared and the effect of calcination temperatures on the Orange II removal was investigated. The raw photocatalysts were activated by calcination at three different temperatures (180 °C, 200 °C and 300 °C) for 1 h duration. Photocatalysts were characterized using thermogravimetric analysis, Fourier-transformed infrared spectroscopy, powder X-ray diffraction and field-emission scanning electron microscopy, high resolution transmission electron microscopy, diffuse reflectance UV–Vis spectroscopy, temperature programed reduction studies and surface area analysis employing Brunauer-Emmet-Teller method. The photocatalytic degradation of Orange II was performed under the irradiation of visible light (500 W halogen lamp) at pH 6.8. The extent of Orange II degradation with initial concentration of 50 ppm was monitored using UV-Vis spectroscopy and at the end of the reaction, total organic carbon analysis (TOC) was conducted. Results from UV-Vis spectroscopy showed that high percentage of Orange II removal was achieved for Cu-Ni/TiO₂ photocatalysts calcined at 180 °C and 200 °C compared to 300 °C. In addition, these photocatalysts also displayed lower TOC values as compared to the photocatalyst calcined at 300 °C. The best performing Cu-Ni/TiO₂ photocatalyst has 9:1 Cu:Ni mass composition and calcined at 180 °C giving 100% Orange II removal with 16.1 ppm TOC value. Although the results from UV-Vis spectroscopy showed 100% Orange II removal, TOC analysis indicated the presence of organic compounds derived from the dye degradation process.

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1. Introduction

The main causes of surface water and groundwater contamination are industrial discharges [1]. The textile industry has a big pollution problem. The World Bank estimates that 17–20% of industrial water pollution comes from textile dyeing and wastewater treatment. Wastewaters generated by the textile industries are known to contain considerable amounts of non-fixed dyes, especially azo-dyes, and a huge amount of inorganic salts. It has been estimated that more than 10% of the total dyestuff used in dyeing processes are released into the environment [2].

Azo dyes are the largest group of synthetic colorants used in textile industry [3] constituting 60–70% of all dyestuffs produced [4]. They have one or more azo groups $(R_1-N=N-R_2)$ having

aromatic rings mostly substituted by sulfonate group $(-SO_3)$, hydroxyl group (-OH), etc. [5,6]. These toxic dyes are nonbiodegradable and at present are abated by some common non-destructive processes [7,8].

Among azo-dyes, Orange II as shown in Fig. 1, represents more than 15% of the world production of dyes used in the textile manufacturing industry. Orange II is an anionic monoazo textile dye of the acid class. It is resistant to light degradation, the action of O_2 and common acids or bases. In wastewater treatment plants, Orange II does not undergo biological degradation [9,10]. The stability of Orange II is useful in textile manufacturing but it causes difficulty in managing its removal. Several techniques have been used to abate the model azo-dye, Orange II, such as Fenton [11], photo-Fenton [12] and TiO₂ photocatalysis [13]. However, these methods are not able to completely remove Orange II from the wastewater system using visible light. Therefore, there is a need to find a new cost effective and efficient technique to eliminate the azo-dye from industrial wastewater.

The removal of azo-dyes by advanced oxidation processes (AOPs) has been the subject of several recent studies. The mechanism of dye destruction in AOPs is based on the formation

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Fig. 1. Chemical structure of Orange II.

of a very reactive hydroxyl radical (•OH), that, with an oxidation potential of 2.80V [14,15] can oxidize a broad range of organic compounds.

 TiO_2 is a very suitable photocatalyst but its activity is mainly confined to the UV region of solar radiation. In order to explore efficient visible light induced photocatalysts, much scientific effort has been conducted in recent years to reduce its band gap to make it suitable for harvesting visible light from solar radiation [6]. These works include: doping TiO_2 with various transition metals such as Pt, Au, and Ag [16,17,18] non metal atoms (N, S, etc.) [19,20] and anchoring an organic dye sensitizer molecule onto the surface of the photocatalyst [9].

The use of Cu and Ni for bimetallic catalyst has been reported as the effective method to improve the efficiency of various reactions. Liu and Liu [21] and Huang and Jhao [22] reported Cu–Ni/Al₂O₃ and Ni–Cu/samaria-doped ceria catalysts for carbon dioxide hydrogenation and for steam reforming of methane, respectively. Other reported studies include decomposition of methane over Ni/SiO₂ and Ni–Cu/SiO₂ catalysts [23], Cu–Ni/TiO₂ [24] prepared via (co)impregnation with 4 wt% loading for photocatalytic reduction of nitrate; Cu–Zn/TiO₂ [25], Ni/TiO₂ [26] and Cu–Fe/TiO₂ [27] for methyl orange degradation and Cu/TiO₂ for Orange II degradation with 90% color removal in the presence of UVC light and O₂ after 150 min reaction [28].

The objective of this paper was to determine the effect of calcination temperature of the bimetallic 10 wt% Cu-Ni/TiO₂ prepared with different Cu:Ni mass compositions on the efficiency of Orange II photodegradation under visible light radiation. The goal was to remove Orange II completely using this new cost effective technique. This involved incorporation of bimetallic Cu-Ni onto TiO₂ via modified deposition-precipitation method (DP) at final pH 8.5. The introduction of Cu and Ni was with the intention to reduce the band gap of the photocatalyst for enhanced visible light absorption. The prepared photocatalysts were further characterized using thermogravimetric analysis (TGA), Fourier-transformed infrared (FTIR) spectroscopy, powder X-ray diffraction (XRD), field-emission scanning electron microscopy (FESEM), high resolution transmission electron microscopy (HRTEM), diffuse reflectance UV-Visible (DR-UV-Vis) spectroscopy, temperature programed reduction (TPR) studies and surface area analysis employing the Brunauer-Emmet-Teller method (BET).

2. Materials and methods

2.1. Materials

Copper nitrate trihydrate, $Cu(NO_3)_2 \cdot 3H_2O$ and nickel nitrate hexahydrate, $Ni(NO_3)_2 \cdot 6H_2O$ (Acros brand >98% purity) were used as dopant metal salts. Titanium dioxide, TiO₂ (Degussa P25 80% anatase, 20% rutile) was used as the support which also acts as the semiconductor in photocatalysis. Sodium hydroxide, NaOH (Merck, 95% purity) was used as precipitating agent. Glycerol used was of 95% purity (Systerm). Orange II (Acros, pure) was used as the model azo dye for photocatalytic degradation study. All chemicals were used as received.

2.2. Preparation of bimetallic photocatalyst

10 wt% Bimetallic Cu–Ni/TiO₂ photocatalysts with varying Cu:Ni mass composition were prepared via precipitation method using NaOH as precipitating agent. The monometallic 10 wt% Cu/TiO_2 and 10 wt% Ni/TiO_2 were also prepared as references. Cu and Ni salts were weighed in appropriate amount and dissolved in 100 ml of distilled water followed by the addition of glycerol in 2:1 mol ratio of glycerol:total metals with continuous stirring [29]. TiO₂ was added to the solution and stirred for 1 h. The pH of the solution was adjusted to pH 8.5 with 0.25 M NaOH. The mixture was stirred at 10 °C for 1 h before filtering and the precipitate was ground with a mortar and pestle, kept in air-tight glass bottle as raw photocatalyst and stored in a desiccator at room temperature prior to calcination.

2.3. Pre-treatment of photocatalysts

In order to estimate suitable calcinations temperatures for the raw photocatalysts, thermal gravimetric analysis (TGA) was carried out using Perkin Elmer (Pyris 1 TGA) instrument. The dried photocatalyst was loaded in a sample cup and weighed using a built-in microbalance attached to the instrument which automatically provide the weight of the sample (in the range of 5–10 mg). The sample was heated in flowing N₂ from 30 °C to 800 °C at a ramp rate of 20 °C/min. Results from TGA were reported as thermograms which are plots of the relative weight of the photocatalyst vs. temperature. Based on the TGA results, calcination was conducted at selected temperatures for 1 h duration. The calcined photocatalysts were given denotation: xCu-yNi-T, where 'x' and 'y' represent the mass composition of Cu and Ni, respectively, with 'x' + 'y' = 10; while 'T represents calcination temperature in °C.

2.4. Characterization of synthesized photocatalysts

It is important to characterize the calcined photocatalysts in order to determine their chemical and physical properties and then to relate these properties to their photocatalytic performance. In this study, photocatalysts were characterized using FTIR (Shimadzu FTIR-8400S), XRD (Bruker D8 Advance Diffractometer), FESEM (Supra55VP), HRTEM (Model: Zeiss Libra 200), DR-UV–Vis (Shimadzu), TPR (Thermo Finnigan TPDRO 1100) and BET surface area analyzer (Micromeritics ASAP 2000).

The phases present in the photocatalysts were investigated using XRD with Cu K α radiation (40 kV, 40 mA) at 2 θ angles from 10° to 80°, with a scan speed of 4° min⁻¹. The morphology of the photocatalysts such as crystallite particle shape, size, and particle size distribution were analyzed using FESEM. DR-UV–Vis measurement was performed using a UV–Vis spectrophotometer equipped with an integrating sphere. Reflectance spectrums were recorded at 190–800 nm wavelength. The band gap energies of the photocatalysts were determined from the reflectance using Kubelka–Munk function, *F*(*R*), and the extrapolation of Tauc plot, which is a plot of (*F*(*R*) · *hv*)^{1/2} against *hv*. Barium sulfate (Ba₂SO₄) powder was used as a standard, an internal reference. Reflectance spectrum was collected as R-sample/R-Reference and then plotted applying Kubelka–Munk Theory in order to determine bandgap energy [32].

2.5. Photocatalytic degradation study

Photocatalytic degradation of 50 ppm Orange II was conducted using halogen lamp (500 W) as the visible light source at 25 °C with an initial solution pH 6.8. Photocatalysts with loading of 1 mg/ml

was added to 10 ml of distilled water and sonicated for 10 min in an ultrasonic bath at 25 °C followed by the addition of Orange II solution to give rise to a final concentration of 50 ppm and volume of 30 ml. The suspension was stirred using a magnetic stirrer for 2 h in the dark and later this suspension was illuminated for 1 h using 500 W halogen lamp as the visible light source at a distance of 25 cm (intensity 30856.66 lux) and the temperature of the reactor was controlled at 25 ± 2 °C by continuous cooling air. During the irradiation experiments, aliquots were withdrawn from the suspension at different intervals and immediately centrifuged to monitor the Orange II concentration and further analysis.

2.6. Orange II concentration monitoring and mineralization

The Orange II degradation during photoreaction was monitored by measuring the solution absorbance from 400 to 800 nm using a Shimadzu UV-3101 UV/Visible spectrophotometer. A calibration curve was obtained beforehand using 1, 10, 20, 30, 50 and 60 ppm standard solutions. Prior to absorbance measurement, the reaction samples were centrifuged twice at 3500 rpm for 10 min to remove the suspended solid photocatalyst. The absorbance peak at 485.0 nm was used as the representative peak for Orange II concentration [30,31]. The photodecolorization efficiency in terms of % Orange II removal was calculated as follows:

%Orange II removal =
$$\left(\frac{C_0 - C}{C_0}\right) \times 100\%$$

where ' C_0 ' is the initial concentration while 'C' is the concentration of Orange II at sampling time.

At the end of the reaction, total organic carbon (TOC) analysis was conducted. TOC (total organic carbon) is an important parameter to assess the organic load of wastewater which provides important information about the presence of certain organic compounds and defined as the amount of carbon bound in an organic compound. Final TOC values in ppm of the reaction samples were taken. Reaction parameters investigated were different Cu:Ni mass compositions, calcination temperatures and irradiation time. Analyses were also conducted for blank experiments where reactions were carried out: without the addition of photocatalyst, with Cu and Ni samples prepared without TiO₂ and with non-modified TiO₂.

3. Results and discussion

3.1. Pre-treatment of photocatalysts

The thermogram of the 9Cu–1Ni/TiO₂ raw photocatalyst is shown in Fig. 2. The TGA curve shows two decomposition steps between 30–180 °C and another at 180–500 °C onwards with total weight loss of 8.98%. The first step is attributed to evaporation of physically absorbed impurities and second decomposition step is attributed for decomposition of Cu(OH)₂ and Ni(OH)₂, respectively. Thus, the proposed decomposition steps for the raw photocatalysts are shown in Eqs. (1) and (2) [32].

$$Cu(OH)_2 \rightarrow CuO_{(s)} + H_2O_{(g)} \tag{1}$$

$$Ni(OH)_2 \rightarrow NiO_{(s)} + H_2O_{(g)}$$
⁽²⁾

Thermograms of the other raw photocatalysts (not shown) with different Cu:Ni mass compositions are similar to that displayed in Fig. 2. Based on the thermogram, three calcination temperatures were selected: $180 \degree$ C, $200 \degree$ C and $300 \degree$ C, for a duration of 1 h.



Fig. 2. Thermogram of 9Cu-1Ni/TiO₂ raw photocatalyst.

3.2. Characterization

3.2.1. Fourier-transformed infrared (FTIR) spectroscopy

Fig. 3 shows the FTIR spectra of the raw and calcined $9Cu-1Ni/TiO_2$ photocatalysts. Several absorption peaks are observed. The broad band around $3400 \, \mathrm{cm}^{-1}$ is attributed to O–H stretching, and the peak near $1600 \, \mathrm{cm}^{-1}$ to O–H bending which is related to physically absorbed moisture. The IR band observed from 400 to $900 \, \mathrm{cm}^{-1}$ corresponds to the Ti–O stretching vibrations [32,33]. The band at $1382 \, \mathrm{cm}^{-1}$ attributed to nitrate (NO₃⁻) group, is present in both raw and calcined photocatalysts even after calcining at 300 °C. Similar band at $1384 \, \mathrm{cm}^{-1}$ was also observed by Li and Inui [34] referred to nitrate which is always present when nitrate salts are used as precursors. No evidence of the presence of Si–OH contamination (sharp band at $3635 \, \mathrm{cm}^{-1}$) in FTIR spectra is observed [35].

3.2.2. XRD

The XRD patterns of bare TiO_2 and $Cu-Ni/TiO_2$ photocatalysts calcined at 200 °C with different Cu:Ni mass compositions are presented in Fig. 4(a). On the other hand, the XRD patterns for Cu-Ni/TiO₂ photocatalysts with 9:1 Cu:Ni mass composition



Fig. 3. FTIR spectra of 9Cu–1Ni/TiO_ photocatalysts: raw (a); and calcined at 180 $^\circ$ C (b), 200 $^\circ$ C (c) and 300 $^\circ$ C (d).



Fig. 4. XRD patterns of bare TiO₂ and Cu-Ni/TiO₂ with (a) different Cu:Ni mass compositions calcined at 200 °C and (b) Cu:Ni mass composition 9:1 calcined at different temperatures (A, anatase, R, rutile).

calcined at different temperatures are shown in Fig. 4(b). No significant differences were detectable for the XRD patterns for all the samples. The main peaks at $2\theta = 25.34^{\circ}$ and 27.46° corresponded to anatase and rutile phases, respectively [32,36,37,38] were present for bare TiO₂ and all the photocatalysts. No phase transition from anatase to rutile was observed for all the calcined photocatalysts, neither the presence of diffraction lines for Cu-and Ni-containing phases. This may indicate high metallic dispersion [39]. Zhu et al. [40] reported that characteristic peaks of metal oxide phase could only be visible when the metal dopant concentration on TiO₂ was above 5 wt%. However, for this paper, at 10 wt% metal loading, the absence of Cu. Ni or mixed Cu-Ni oxide phases clearly indicated that the dopants were well dispersed on TiO₂. This may be due to the use of glycerol during photocatalyst preparation that favored the formation of small metal particles since it has been reported that glycerol prohibited the aggregation of metal particles [41].

3.3. Photocatalyst morphology: FESEM and HRTEM

Morphology of the photocatalyst often plays important role in its catalytic properties. The particle size has an important influence on the photocatalytic process due to changes in transmission, dispersion and absorption of light, and in the catalyst surface availability. The FESEM micrographs of the prepared photocatalysts with different Cu:Ni mass compositions as shown in Fig. 5, clearly depict uniform distribution with irregular sized spherical morphologies with slight agglomeration ranging from 11 to 35 nm. Yoong et al. [32] and Nurlaela et al. [39,42] also reported similar results of agglomeration for Cu/TiO₂.The degree of agglomeration for the photocatalyst with Cu:Ni mass composition 9:1 was higher when calcined at 300 °C when compared to that calcined at 200 °C. This may be due to sintering during calcination process [42]. It was observed from EDX mapping (Fig. 5b) of the photocatalysts that the dopant metals were uniformly dispersed onto the support. These findings are in agreement with the XRD results indicating that the doped metals were well dispersed onto the support.

In this work, HRTEM was used to obtain more detailed discernable microstructure information in order for single grains and grain boundaries to be accurately analyzed. The Cu–Ni/TiO₂ photocatalysts samples calcined at 200 °C and bare TiO₂ were analyzed using HRTEM to obtain crystallite size and morphology. As shown in Fig. 6, the HRTEM micrographs display very good crystalline morphology of the particles with irregular morphology. The size of the particles were in the range of 11–30 nm for Cu–Ni/TiO₂ and 11–35 nm for bare TiO₂. Results are in good agreement with the FESEM data in terms of the metal particles morphology.



Fig. 5. (a) FESEM micrographs of bare TiO₂, Cu–Ni/TiO₂ with different Cu:Ni mass compositions calcined at 200 °C and 9Cu–1Ni mass composition calcined at 300 °C (150k×). (b) EDX and Mapping image of 9Cu–1Ni/TiO₂ photocatalysts.



Fig. 6. HRTEM micrographs of bare TiO2 and Cu-Ni/TiO2 with different Cu:Ni mass compositions calcined at 200 °C (50 nm).

3.3.1. Diffuse reflectance UV–Visible (DR-UV–Vis) spectroscopy

One of the challenges in the development of TiO₂ is to shift the absorption spectrum of TiO₂ into the visible region to enable more efficient sunlight harvesting. In this work, incorporation of bimetallic Cu–Ni onto TiO₂ was chosen for this purpose. In order to determine the band gap energy of the photocatalysts, DR-UV–Vis was conducted. The DR-UV–Vis spectra of bare TiO₂ and Cu–Ni/TiO₂ photocatalysts with different Cu:Ni mass compositions are presented in Fig. 7. DR-UV–Vis spectrum of bare TiO₂ showed absorption peaks ranging from 190 nm and 400 nm, similar to that observed by Yoong et al. [32] and Nurlaela et al. [39]. The absorption at 323 nm is generally related to the electronic excitation from O 2p valence band to Ti 3d conduction band indicating that Ti presents as tetrahedral Ti⁴⁺ species [43]. The activities of the



Fig. 7. Absorption spectra of bare TiO_2 and $Cu-Ni/TiO_2$ calcined at 200 °C with different Cu:Ni mass compositions.

prepared photocatalysts as compared to bare TiO₂ are presented in Table 1. The light absorption properties of TiO₂ modified with Cu–Ni was enhanced significantly. The band gap energies of the photocatalysts (Fig. 8) were determined from the Tauc plot, a plot of $(F(R) \cdot h\nu)^{1/2}$ against $h\nu$. F(R) is the Kubelka–Munk function derived from reflectance spectra where $F(R) = (1 - R)^2/2R$ equation, and $h\nu$ is the photon energy.

3.3.2. Temperature programed reduction (TPR)

The TPR profiles of the photocatalysts are presented in Fig. 9. TPR was employed to characterize the Cu–Ni/TiO₂ photocatalyst with respect to the type of metal oxide species present, either copper oxide, nickel oxide, or copper–nickel mixed oxide, and the degree of interaction of the oxides with TiO₂ support [32]. The reduction profile of bimetallic photocatalyst with 9:1 and 1:9 Cu–Ni mass compositions showed similar reduction peaks at 294 °C while for 5Cu–5N–200 reduction peaks was at 308 °C with a shoulder around 444 °C.

The reduction profile of Cu–Ni/TiO₂ calcined at 200 °C with 9:1 and 1:9 Cu:Ni mass compositions displayed reduction peak at 294 °C correlating to reduction of CuO with strong interaction with TiO₂ [44] or might be attributed to the reduction of Cu–Ni

Calculated band gap energies of bare TiO ₂ and Cu–Ni/TiO ₂ photocatalysts.	ble 1	
	lculated band gap energies of bare TiO_2 and $Cu-Ni/TiO_2$ photocatalysts.	

Photocatalyst	Bandgap energy (eV)	% Orange II removal	TOC
Bare TiO ₂	3.16	21	55.7
10Cu-0Ni-200	2.90	54.9	19.1
9Cu-1Ni-200	3.0	100	20.2
7 Cu-3Ni-200	3.1	63	18.8
5Cu-5Ni-200	3.0	100	21.9
3Cu-7Ni-200	3.0	97.3	23.2
1Cu-9Ni-200	2.97	90.4	27.8
0Cu-10Ni-200	3.14	46.7	25.2



Fig. 8. (a) and (b) Plot of transformed Kubelka–Munk functions $[F(R) \cdot hv]^{1/2}$ vs. hv for bare TiO₂ and Cu–Ni/TiO₂ calcined at 200 °C with different Cu:Ni mass compositions.

mixed oxide instead of individual oxide. It is observed that the reduction peak and shoulder for CuO are shifted to higher temperature. The small shoulders below 250 °C might be attributed to the reduction of highly dispersed CuO with less interaction with the TiO₂ support [32,45] and also correspond to Cu(II) reduction to Cu(0) [46]. Apparently, smaller CuO particles were formed on the surface of photocatalyst, decreasing the reduction temperature. The 5Cu–5Ni–200 displayed a peak at 308 °C attributed to the reduction of NiO having strong interaction with TiO₂ [47]. The weaker shoulder at 444 °C corresponded to the well dispersed NiO with weak metal–support interaction [42]. With respect to the different Cu:Ni mass compositions only small differences were observed. In Fig. 9(b), reduction peaks can be easily differentiated for the monometallic Cu/TiO₂ and Ni/TiO₂ photocatalysts calcined at 200 °C, with 282 °C for bulk CuO, 347 °C and 462 °C for bulk NiO.

3.3.3. The surface area of photocatalyst

The BET surface area, pore volume, and pore diameter of bare TiO_2 and $Cu-Ni/TiO_2$ photocatalysts with different Cu:Ni mass compositions are shown in Table 2. All the samples displayed Type IV isotherms with hysteresis loops, which indicates capillary condensation in mesoporous adsorbate [48,49,32,39]. TiO_2 displayed type III pattern, which is typically ascribed to non-porous products with weak interactions between the adsorbent and the adsorbate. With reference to the effect of Cu:Ni mass compositions on surface area, all the supported bimetallic photocatalysts have specific surface area of ~43 m² g⁻¹. However, no clear trend could be deduced for the total surface area of the photocatalysts. The surface area increased with Cu content but at high Ni loading, a decrease in surface area was observed. Average pore diameter increased with the increase in Ni contents and decrease of Cu contents.



Fig. 9. The TPR profiles of (a) $Cu-Ni/TiO_2$ photocatalysts with different Cu:Ni mass compositions calcined at 200 °C and (b) 10 wt% monometallic and bimetallic Cu-Ni/TiO₂ photocatalysts calcined at 200 °C.

In case of calcination temperature, the surface area and pore volume increased with calcination temperature while the pore diameter of photocatalyst decreased with increasing temperature as shown in Table 2. However, the BET surface area reached the maximum $(51.8 \text{ m}^2 \text{ g}^{-1})$ for photocatalyst with 5:5 Cu:Ni mass composition calcined at 300 °C. High metal dispersion on the TiO₂ surface was reported when the total surface area of photocatalysts was increased [42]. With reference to the degradation reaction study as shown in Fig. 10(a), the results of photocatalyst with 5Cu:SNi mass composition calcined at 200 °C (with the highest BET surface area) displayed almost similar performance in terms of TOC results as compared to Cu:Ni; 9:1 and 1:9 photocatalysts,

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The BET surface area of bare TiO_2 and $\mathrm{Cu-Ni}/\mathrm{TiO}_2$ photocatalyst.	
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Photocatalyst	BET surface area (m ² g ⁻¹)	Total pore volume $(cm^{-3}g^{-1})$	Average pore diameter (nm)
Bare TiO ₂	43.1	0.20	18.5
9Cu-1Ni-180	42.5	0.29	27.7
9Cu-1Ni-200	43.2	0.21	19.5
9Cu-1Ni-300	49.9	0.28	22.6
5Cu-5Ni-180	45.4	0.29	25.9
5Cu-5Ni-200	45.6	0.38	33.7
5Cu-5Ni-300	51.8	0.28	21.7
1Cu-9Ni-200	43.4	0.36	33.9



Fig. 10. (a) Photocatalytic degradation of Orange II using bare TiO₂ and Cu–Ni/TiO₂ photocatalysts with different Cu–Ni mass compositions. (b) Photocatalytic degradation of Orange II using Cu–Ni, bare TiO₂, Cu/TiO₂, Ni/TiO₂ photocatalysts and Orange II solution without TiO₂.

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indicating that surface area may not be the major factor responsible for the photocatalytic activity.

3.4. Orange II concentration monitoring and mineralization

3.4.1. Effect of Cu:Ni mass composition

Results from the effect of different Cu:Ni mass compositions on Orange II degradation are presented in Fig. 10(a), (b) and Table 3. Photocatalysts calcined at $200 \,^\circ$ C showed 100% dye removal for Cu:Ni mass compositions of 9:1 and 5:5 as shown in Fig. 10(a). However, photocatalysts with 3:7 Cu:Ni mass composition showed 97.3% Orange II removal. In the case of photocatalysts with 7:3 and 1:9 Cu:Ni mass composition, lower dye removal activity was observed compared to the other photocatalysts with different Cu:Ni mass compositions. The degradation activity decreased further to 90.4% and 63.0% for photocatalysts with 1:9 and 7:3 mass compositions, respectively.

At lower calcination temperature ($180 \,^{\circ}$ C), the photocatalysts displayed better activity with 100% Orange II removal for photocatalysts with 9:1, 5:5 and 1:9 Cu:Ni mass compositions (Table 3). For photocatalyst with 3:7 Cu:Ni mass composition, it showed higher activity (93.3%) compared to that with 7:3 Cu:Ni mass composition (75.2%). For the photocatalysts calcined at 300 °C, the Orange

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Removal of Orange	II and TOC values.

Cu:Ni ratio	Cal. temperature	% Removal	TOC (ppm)
(9:1)	180	100.0	16.1
(7:3)	180	75.2	20.2
(5:5)	180	100.0	64.7
(3:7)	180	93.3	22.5
(1:9)	180	100.0	26.1
(9:1)	200	100.0	20.2
(7:3)	200	63.0	18.8
(5:5)	200	100.0	21.9
(3:7)	200	97.3	23.2
(1:9)	200	90.4	27.8
(9:1)	300	57.1	45.8
(7:3)	300	76.0	42.1
(5:5)	300	72.0	44.2
(3:7)	300	58.0	43.6
(1:9)	300	66.5	42.3
(10:0)	200	54.9	19.1
(0:10)	200	46.7	25.2
Bare TiO ₂	_	21	55.7
Cu-Ni	200	3.2	-
No photocatalyst	-	3.0	36.7

TOC, total organic carbon.

II removal was in the range of 57.1–76.0%, the highest displayed by photocatalyst with 7:3 Cu:Ni mass composition.

In terms of dye mineralization, only photocatalysts with 100% Orange II removal were taken into consideration. Even though results from UV-Vis spectroscopy showed complete Orange II removal, TOC analysis registered the presence of organic compounds which were derived from the dye degradation process. For 200 °C calcination temperature (Fig. 10(a)), photocatalysts with 9:1 and 5:5 Cu:Ni mass compositions displayed TOC values of 20.2 ppm and 21.9 ppm, respectively. The photocatalysts calcined at 180 °C which showed complete removal of Orange II were those with 9:1, 5:5 and 1:9 Cu:Ni mass compositions, and the displayed TOC values were 16.1 ppm, 64.7 ppm and 26.1 ppm, respectively. Monometallic 10 wt% Cu/TiO₂ and 10 wt% Ni/TiO₂ photocatalysts with 10:0 and 0:10 Cu:Ni mass compositions, respectively, displayed much lower activity compared to the bimetallic catalysts but showed higher Orange II removal compared to bare TiO₂. Furthermore, activity of monometallic Cu/TiO₂ (54.9%) was reported with better performance compared to and Ni/TiO₂ (46.7%). Therefore, the presence of bimetallic Cu-Ni displayed synergistic effect for dye removal. Results with improved activity for TiO₂ doped with Cu and Ni, were reported for Cu–Ni/TiO_2 [42] for hydrogen production and NixCuy/Al₂O₃ [50], methanol steam reforming, photocatalytic reduction of nitrate [24], Orange II degradation [51,52] with respect to the monometallic ones.

Blank experiments were also conducted for comparison purposes. Orange II solution (50 ppm) without the addition of any photocatalyst (No photocatalyst) with the addition of TiO₂ (Bare TiO₂) was chosen for blank experiments. The bimetallic Cu-Ni prepared in the same conditions as for the Cu-Ni/TiO₂ photocatalysts but in the absence of TiO₂ (Cu-Ni) was also considered. The activities of these samples were compared with the monometallic 10 wt% Cu/TiO₂ (10Cu-0Ni-200) and 10 wt% Ni/TiO₂ (0Cu-10Ni-200) photocatalysts in Fig. 10(b). Bare TiO₂, monometallic 10 wt% Cu/TiO₂ and 10 wt% Ni/TiO₂ photocatalysts displayed 21.0%, 54.9% and 46.7%, respectively, of Orange II % removal. However, in the absence of TiO₂, Orange II removal was negligible, giving 3.0% and 3.2%, for "No photocatalyst" and Cu-Ni, respectively. This indicates that the active material for photodegradation of Orange II is TiO₂ and bimetallic Cu-Ni acts as modifier to reduce the band gap of TiO₂ [42].

In the present study, compared to monometallic Cu/TiO₂ and Ni/TiO₂ photocatalysts, Bimetallic Cu–Ni/TiO₂ photocatalysts showed better photocatalytic activity in terms of Orange II % removal as shown in Table 3. Furthermore, activity of monometallic photocatalysts in terms of Orange II degradation, Cu/TiO₂ (54.9%) was reported with better performance compared to and Ni/TiO₂ (46.7%). These results conform to the previous studies reported for the enhanced photoactivity for the bimetallic Cu–Ni/TiO₂ photocatalyst by Gao et al. [24], Nurlaela et al. [39], Riaz et al. [51] and Riaz et al. [52].

Changes in the catalytic properties induced by adding Cu to Ni is caused by changes in the electronic properties of the homogeneous alloy particle, by the formation of active surface structures, by preferential segregation of one metal to the surface or by a combination of all these effects [22,53,54]. The catalytic properties of bimetallic nanoparticles are directly related to their structure and composition which may be controlled by processes taking place during catalyst preparation [55]. For example, even though Cu has a lower surface free energy than Ni and should, based on thermodynamics, preferentially occupy surface sites [56], core-shell structures with Ni surface enrichment [53] or Cu surface enrichment [54] does occur. For a tiny metal-modified semiconductor particle, supported bimetal Cu and Ni can behave as short-circuited photoelectrochemical cell, where both cathodic and anodic reactions can occur on the same particle [57]. For photogenerated electrons and holes, metal Ni and Cu in the semiconductor surface can separately trap these reductive electrons and oxidative holes and prevent their combinations, then transfer these trapped electrons or holes to absorbed substances in their surface, thereby increase their existent life and improve the efficiency of a photocatalytic reaction. It has also been reported that the Cu²⁺ doped TiO₂ catalyst increased the photocatalytic degradation of two typical azo dyes used in dyeing industry namely Orange II and Tartrazine (Tart) [58]. The behavior of Cu²⁺ was explained on the basis that Cu²⁺ may scavenge electrons resulting in the formation of Cu⁺, which in turn enhances the oxidation of the substrate [59].

In the present research, XRD patterns, Fig. 4(a) and (b) of Cu-Ni/TiO₂ photocatalyst showed only the main characteristic peaks of TiO₂ support, no phase transition from Anatase to rutile and characteristic reflections for Ni, Cu or their Cu-Ni combination (alloy) containing phases are observed. These results were further confirmed by FESEM analysis which indicates that metal particles are well dispersed or interact with TiO₂ support. The interaction with the support and the concomitant presence of the two metals strongly promoted the reducibility of the material [50]. Previously it was also reported that the catalytic performance of bimetallic systems was promising in the methanol stream reforming [50] and reduction of nitrate into nitrite [24]. The Introduction of copper in the catalyst formulation showed excellent performance and furthermore this promoting effect of bimetal is probably attributed to the more effective separation of photogenerated spatial charges in tiny TiO₂ semiconductor particles [24].

3.4.2. Effect of calcination temperature

10 wt% Bimetallic Cu–Ni/TiO₂ photocatalysts calcined at three different temperatures (180, 200 and 300 °C with calcination duration 1 h) is studied for Orange II degradation. High percentage removal of Orange II is observable using Cu–Ni/TiO₂ calcined at 180 °C and 200 °C in the range 63–100% giving TOC values of 16.1 ppm to 64.7 ppm, after 1 h of reaction (Table 3). At higher calcination temperature (300 °C), lower performance is observed from 57.1% to 76% dye removal with 42.1–45.2 ppm TOC values. The reaction using TiO₂ standard displayed the lowest Orange II removal (21%) with very high TOC value (55.7 ppm).

Photocatalysts calcined at $180 \,^{\circ}$ C and $200 \,^{\circ}$ C showed 100%Orange II removal for 9:1 Cu:Ni mass compositions with 16.1 and 20.2 ppm TOC value. For the 9:1 Cu:Ni mass composition, at higher calcination temperature ($300 \,^{\circ}$ C), lower dye degradation was observed with only 57.1% Orange II removal and 45.2 ppm TOC value.

3.4.3. Effect of irradiation time

Fig. 11 displayed the % Orange II removal as a function of time (120 min dark reaction followed by 60 min light reaction) for photocatalysts with 9:1 Cu:Ni mass composition. During dark reaction, decolorization was the fastest for photocatalyst calcined at 180 °C compared to the other temperatures. It was already 100% after 60 min in the dark without exposure to irradiation indicating high dye adsorption rate. For photocatalyst calcined at 200 °C, Orange II removal was observed even in the dark, and the removal progressed to 85.5% after 120 min in the dark. The degradation progressed further to 100% after 60 min irradiation. However, for photocatalyst calcined at 300 °C and bare TiO₂, degradation rate was very slow (40.0%) compared to other two photocatalysts. It is evident that the percentage of decolorization and photodegradation increases with irradiation time for photocatalysts calcined at 200 °C and 300 °C. Photocatalysts calcined at 300 °C showed less adsorption during dark reaction but the rate of reaction during irradiation was comparable to that for photocatalyst calcined at 200 °C. The reaction rate during light reaction decreases with irradiation time as it follows the pseudo first-order kinetics and additionally a competition



Fig. 11. Orange II degradation in the dark and with radiation using photocatalysts with 9:1 Cu:Ni mass composition calcined at different temperatures.

for degradation may occur between the reactant and the intermediate products. The slow kinetics of dye degradation after certain time limit is mainly attributed to: (a) the difficulty in converting the N-atoms in Orange II into oxidized nitrogen compounds [60], (b) the slow reaction of short chain aliphatics with •OH radicals [61] and (c) the short life-time of photocatalyst because of active sites deactivation by strong by-products deposition (carbon, etc.) [62].

Photocatalysis is a surface phenomenon, a critical step in intervening in the effectiveness of photodegradation is adsorption of pollutants on the photocatalyst surface [63]. Many workers measured the adsorption and the kinetics of photodegradation of different compounds on TiO₂ photocatalyst, such as phenol [64] and Methylene Blue [65], 2-chlorophenol [66], Reactive Black [65,67] and monoazo dye (Reactive Red 198), poliazo dye (Direct Green 99) [63] and supported TiO₂ catalyst for Orange II [68].

In all the cited studies, organic compounds are adsorbed on the photocatalyst surface to some degree. The adsorption process proceeds to reach an equilibrium and then lamps are switched on and the photocatalysis process is conducted. In the case of dyes, there may be some problems to distinguish the adsorption of dyes on the photocatalyst surface from the photocatalytic decomposition of the dyes. There is no problem if the adsorption of the dye on the surface of TiO_2 is negligible [69,70].

A comparison study was performed using bare TiO_2 and $Cu-Ni/TiO_2$ separately, which showed overall removal of Orange II by $Cu-Ni/TiO_2$ photocatalysts was considerably higher than that of bare TiO_2 . All the experiments were performed under natural pH condition (pH 6.8) using 50 ppm of Orange II, and 1 mg I^{-1} of photocatalysts indicate that effective surface area (Table 2) and adsorption capacity of the synthesized $Cu-Ni/TiO_2$ were much higher than bare TiO_2 , which favor rapid removal of Orange II from the solution.

Although all the supported catalysts showed very good adsorption characteristics compared to that of bare TiO_2 , pure support (bare TiO_2) with surface area 43.1 m² g⁻¹ showed very poor adsorption of Orange II. Orange II being slightly acidic and anionic is subjected to electrostatic repulsion and the negative surface of the support.

4. Conclusion

Bimetallic Cu–Ni/TiO₂ photocatalysts were prepared with different Cu:Ni mass compositions and calcined at different

temperatures. In the present work, Cu–Ni/TiO₂ photocatalysts displayed better photocatalytic activity of as high as 100% Orange II removal as compared to bare TiO₂ which displayed only 21.0%. The XRD patterns of the bimetallic photocatalysts did not show the presence of separate metal diffraction peaks for Cu or Ni phases. This is mainly due to the high metal dispersion of the metals onto TiO₂. Results from the XRD and FESEM analyses were in favor to the metal particles existing in the form of well dispersed oxides on TiO₂.

The reduction profile (TPR) of bimetallic photocatalyst showed similar reduction peaks indicating the presence of Cu and Ni mixed oxides. Surface area of photocatalysts was almost similar to the bare $TiO_2 \sim 43 \text{ m}^2 \text{ g}^{-1}$ except for 5:5 Cu–Ni ratio, observed with higher surface area. The photocatalyst performance of the bimetallic system is promising compared to bare TiO_2 and the monometallic photocatalysts. Decolorization was faster for $180 \,^\circ\text{C}$ compared to other calcination temperatures which may be due to the increased pore diameter. The best performing Cu–Ni/TiO₂ photocatalyst has 9:1 Cu:Ni mass composition and calcined at $180 \,^\circ\text{C}$ giving 100% Orange II removal with 16.1 ppm TOC value. Although the results from UV–Vis spectroscopy showed 100% Orange II removal, TOC analysis indicated the presence of organic compounds derived from the dye degradation process.

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Appendix A. Supplementary data

Supplementary data associated with this article can be found, in the online version, at doi:10.1016/j.cej.2012.01.052.

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